HALF YEARLY ENVIRONMENTAL DATA GENERATION REPORT

Period: October 01, 2023 to March 31, 2024 For



HALDIA PETROCHEMICALS LIMITED HALDIA: PURBA MEDINIPUR: WEST BENGAL



Monitoring Agency





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West Bengal Pollution Control Board (Department of Environment, Govt. of West Bengal) Memo No. 3664-5/WPB-S/99 (Part-VI), Validity: upto 30.06.2024.

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Recognised by National Accreditation Board for Testing and Calibration Laboratories (NABL), Accreditation Standard ISO/IEC 17025:2005, Certificate Number TC-7649, Validity 22.03.2023 to 21.03.2025.

Recognised by MoEF & CC, Govt. of India for Air, Effluent and Drinking Water Quality Testing up to 11.04.2024 vide The Gazette of India, Extraordinary, Part—II, Section—3, Sub-Section(ii), F. No. Q-15018/61/2018 - CPW Dated — 13.12.2019.





PREFACE

Haldia Petrochemicals Limited, one of the largest petrochemical complexes in India and the only one of its kind in eastern region. The complex produces ethylene, propylene and associated liquid stream products for downstream processing into polymers and chemicals.

The scope of the study includes detailed characterisation of the environment in and around HPL complex covering an area of 10-km radius from the center of the HPL plant for Air, Noise, Effluent etc. Scientific Research Laboratory established an Environmental Laboratory in HPL Plant premises for this purpose. All sampling and testing were performed by following well-established and recognized standard procedures.

Scientific Research Laboratory wishes to place on record its deep appreciation for the trust reposed in Scientific Research Laboratory by Haldia Petrochemicals Limited for carrying out this study. Our heartiest thanks go to Mr. Sanjaya Bhatnagar, EVP & Head Plant and Mr. Praveen Jain, Head - HSEF for their kind cooperation & help provided during the course of study.

We also appreciate tireless efforts of Mr. Subandhu Bhattacharya, Sr.Manager – Environment Services & Mr. Saugata Mahindar, DGM -Environment Services without whom it would not have been possible to bring out the final report.

Prepared By

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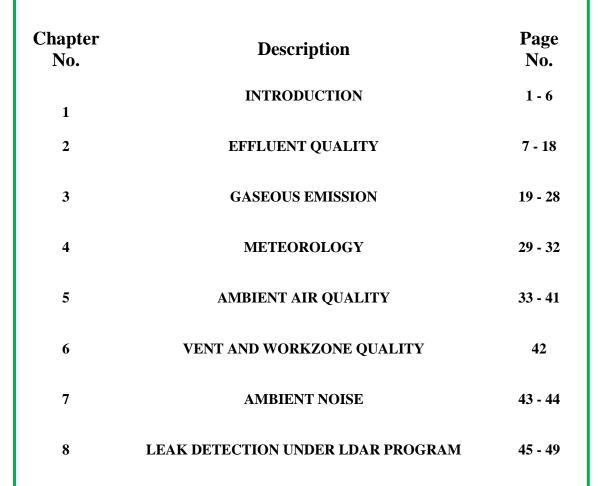
Approved by

(Dr. Jyotirmoy Majumdar) Chief Executive





CONTENT



CHAPTER NO. - 01 INTRODUCTION

HALDIA PETROCHEMICALS LIMITED - SATELLITE IMAGE



Page - 01





1.0 INTRODUCTION

1.1 General

Haldia Petrochemicals limited (HPL), Haldia, West Bengal is an integrated Petrochemicals production unit and only petrochemical complex in West Bengal. HPL mainly comprises of Naphtha Cracker Unit (NCU), Pyrolysis Gasoline Hydrogenation unit (PGHU), Py-gas Desulfurisation (PGDS), Butene-1, Benzene Extraction Unit (BEU), Butadiene Extraction Unit (BDEU). The down stream units comprise of Linear Low Density Poly Ethylene (LLDPE), High Density Poly Ethylene (HDPE) and Poly Propylene (PP).

HPL is located at about 58 nautical miles by waterways and 130 Km by roadways from Calcutta and lies in the Haldia Industrial area. Haldia is in Purba Medinipur district, West Bengal between at latitudes 21°56′10″ (N) and longitude 88°5′47″ (E). The site lies adjacent to the road linking SH 4 and NH 41. Nearest railway, station is Durgachak on the Panskura – Haldia branch line of SE railway.

A comprehensive Environmental Impact Assessment Studies for the Haldia Petrochemicals Complex was carried out in 1991. Due to the rapid urbanisation and industrialisation, the environmental scenario of this area has changed in many respects. HPL started commercial production from the month of August 2001. HPL has entrusted Scientific Research Laboratory, Kolkata, the job of Environmental Data Generation in respect of air, water, noise and solid waste after commissioning of their petrochemical complex at Haldia.

1.2 Study Area

Keeping in view the nature and size of the complex, the various guidelines available, past experience and the original EIA report, it was decided to cover an area of 10 km. radius for the purpose of ambient air monitoring from the center of the plant. Study area covers 196 villages. Field data collection are restricted within the 10 km. radius of the plant center.

1.3 Objective of The Study

The purpose of the present study is to assess the effect of industrial activity on the environment at Haldia. The availability of resources in this area is the result of the interaction between the physical occurrence and the amount of requirement and economic means of their exploitation. Haldia is one of the most industrialized zones in the Bank of Hoogly River. The area has neither rapid industrial growth nor causes serious ecological/environmental imbalance bringing resultant problems. Ambient air quality with respect to PM_{2.5}, PM₁₀, SO₂, NOx, CO, Benzene, B(a)P, As, Ni, Pb, NH3 & O3 has been monitored to evaluate the environmental conditions in and around the complex. These monitoring will help to assess the environmental scenario after commissioning of HPL also.





The Environmental Data Generation work has been undertaken by Laboratory of **Scientific Research Laboratory**, **Kolkata** for the following:

- Evaluation of present environmental status through comprehensive analysis of various generated & collected environmental data.
- Predict the probable impact on the various environmental factors due to the HPL operation.
- Analysis of the predicted impact vis-à-vis the regulatory environmental standards.
- Assessments of efficacy in process and pollution control systems.

1.4 Contents of the Report

Environmental monitoring for generation of data on meteorology, ambient air and effluent were carried out for the months of **October 2023 to March 2024**. This report contains the data of meteorology during the ambient air monitoring, analysis report of ambient air quality, work zone monitoring results, stack monitoring data, ambient Noise monitoring report, LDAR and effluent analysis report with respect to MoEF & CC and WBPCB parameter specified for Petrochemical industries and HPL respectively.

1.5 Location of the Site

Haldia Petrochemicals complex is in the industrial area of Haldia, which is developed by Haldia Development Authority. Haldia is situated at latitudes 21°56′10″(N) and longitude 88°5′47″ (E) on the confluence of Hoogly and Haldi river in Purba Medinipur district, West Bengal. It is about 58 nautical miles by waterways and 130 km. by roadways from Calcutta. The area is well connected with roads, waterway and railways.

The site is flat and plain, typical of the Ganges's of the delta region. Up to the late 1960s, what is now Haldia was a very rural area. There was small set up of the Calcutta port from sand Heads and back. This was called the "Anchorage Camp" and was near the mouth of the Haldi River. With adequate favorable infrastructure such as roads, railways, waterways, port and power, Haldia has now become a major industrial township in west Bengal, after Durgapur – Asansol region. Haldia planning area is governed by Haldia Notified Area and is bounded by Hooghly, Haldi and Hijli river tidal canal. The total area of Haldia Notified Area is about 326.85 sq. km.





1.6 Major details of industries, which are contributing to pollution load in Haldia, its distance and location with respect to HPL Complex, are as follows:

Sl. No.	Name of the Industry	Distance from HPL complex	Direction with respect to HPL
1	Adani Wilmer Ltd.	1.0 km	North- West
2	Dhunseri Petrochem & Tea Ltd.	1.0 km	North-East
3	DPM Net Pvt. Ltd.	1.5Km	North
4	Exide Industries Ltd.	2.6 km	East
5	Emani Biotech Ltd.	2.0 km	East
6	Ennore Coke Private Ltd.	4.0 km	East ,North- East
7	Electrosteel Casting Ltd.	0.8 Km	North
8	Gokul Refoils & Solvent Ltd.	2.0 km	North- West
9	Greenways Shipping Agencies Pvt. Ltd.	3.5 km	North- West
10	Hindustan Unilever Ltd.	3.5 km	East
11	Hooghly Met Coke & Power Company	1.7 Km	South
12	Indian Oil Corporation Ltd., Haldia Refinery	3.6 km	South
13	IOC Petronas Ltd.	0.6 km	North
14	KoPT/Haldia Dock Complex	4.5 km	South
15	Lalbaba Seamless Tubes Pvt. Ltd.	1.5 km	North- West
16	MCC PTA India Corp. Private Limited	4.0 km	East ,North- East
17	M/S West Bengal Waste Management Ltd.	2.5 Km	North-East
18	Manaksia Ltd.	4.2km	East ,North- East
19	Marcus Oils Chemical Pvt. Ltd.	0.5 km	North
20	Ruchi Soya Industries Limited	0.5 km	South
21	Reliance Petroleum Ltd.	1.0 km	North
22	R.D.B. Rasayans Ltd.	0.5 km	East
23	SWAL Corporation Ltd.	2.5 km	East
24	Shamon Ispat Ltd.	2.3 km	North- West
25	Shree Renuka Sugars Ltd.	1.5 Km	South- West
26	Sanjana Cryogenic Storages Ltd.	3.5 km	East
27	Tata Chemicals Ltd.	3.0 km	East





Industrial map







1.7 Site Environmental Monitoring

Site Environmental monitoring was carried out for six months (October 2023 to March 2024) through out the year comprising of two seasons as per MOEF & CC guidelines such as Sumer & Monsoon season in respect of

- Effluent Quality
- Stack Emission
- Meteorology
- Ambient Air Quality
- Work Zone Air Quality
- Ambient Noise
- LDAR Program

Monitoring was started in the month of **October 2023**. The purpose of the environmental monitoring was just to know environmental scenario in and around the HPL complex. Results of baseline studies are summarized in relevant chapters.

CHAPTER NO. - 02

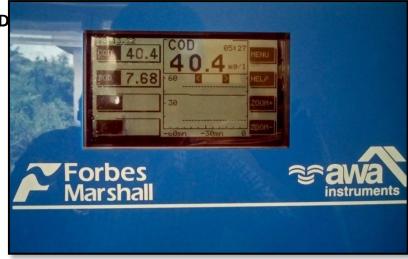
EFFLUENT QUALITY





Online Treated Effluent Monitoring System





Online TSS analyser







2.0 EFFLUENT QUALITY

HPL generates liquid waste water from Naphtha Cracker Unit, Butadiene Extraction Unit, Pyrolysis Gasoline Hydrogenation Unit, Benzene Extraction Unit, HDPE, LLDPE, PP, Cooling Tower, DM Water Plant, utilities and off site buildings. The waste-water generated requires suitable treatment before disposal and a comprehensive waste water management system comprising of collection, treatment, and disposal facilities are provided.

The treatment facilities are divided into two distinct sections, namely, pre- treatment section inside battery limits (ISBL) of the respective units and final treatments in Waste Water Treatment Plant (WWTP)

ISBL Treatment is provided for the following streams

- Spent caustic stream from Naphtha Cracker Units (NCU)
- Neutralization / free oil removal in NCU.
- Polyethylene Plants/Polypropylene Plant ISBL units for removal of Polymers and oil.
- Neutralization for Demineralisation of water plant

WWTP has been broadly designed for following treatment systems

- Oil Recovery System
- Contaminated Rain Water Treatment System
- Sanitary Sewer Treatment System
- Biological Treatment System
- Slop Oil Collection System
- Sludge Handling System
- Final Discharge System

2.1 PRETREATMENT FACILITIES

Spent Caustic from Cracker Unit

Spent caustic stream emerging from cracker unit are highly alkaline and contains high oxygen demand. In the spent caustic treatment plant, Na₂S is converted to sodium thiosulphate by oxidation process. After this treatment the stream is sent to WWTP.

Polyethylene Plants/ Poly Propylene Plant

Wash water and effluent streams from process contain trace hydrocarbon and polymers, which are collected in ISBL and then sent to WWTP after oil skimming and removal.





2.2 DETAILS OF WASTE WATER TREATMENT PLANT

The treatment facilities are designed for treating process water for reduction of free and emulsified oil, sulphide, phenol, thiosulphate, total suspended solids (TSS), bio-chemical oxygen demand (BOD), chemical oxygen demand (COD) and the contaminated rain water for removal of oil and suspended solids. The treated effluents from WWTP are meeting the discharge standards stipulated by West Bengal Pollution Control Board.

The wastewater treatment plant consists of Physical, Chemical and Biological treatment facilities for removal of oil, suspended solids and biodegradable organic.

Treatment Scheme of WWTP

The physical and chemical treatment scheme consists of the following units:

- Bar Screen and Grit Chamber
- Tilted Plate Interceptor (TPI)
- Equalization Tank
- pH Adjustment Tank
- Flash Mixing Tank
- Flocculation Tank
- Dissolved Air Flotation System

The biological treatment scheme consists of following units:

- Aeration tank
- Secondary Clarifier

The slop oil handling facility consists of the following units:

- Oil Skimmer
- Slop Oil Tank
- Wet slop oil sump

The sludge, handling facility consists of the following units:

- Chemical & Oily Sludge Sump
- Bio-Sludge Sump
- Thickener
- Thickened Sludge Sump
- Centrifuge





The treatment scheme for treating contaminated rainwater during wet weather flow consists the following units:

- Wet Weather Flow (WWF) Receiving sump
- Screen Chamber
- Grit Chamber
- Surge Pond
- Contaminated Rain Water (CRW) Transfer Sump
- TPI

WWTP has been broadly designed for following treatment systems:

Oil Removal / Recovery system

Pretreated effluent streams from various units are routed to TPI Separators for removal of free oil and suspended solids. The free oil removed from the TPI Separators, is being collected in the wet slop oil sump. The oily sludge from the bottom of TPI separators is routed to the chemical and oily sludge sump. Then the effluent from TPI units is routed (by gravity) to the equalization tank for equalization of flow and modulation of characteristics. Floating oil skimmer is provided to remove the free-oil layer formed in equalization tank. This free oil is being routed to the wet slop oil sump.

HDPE process effluent is directly received to the equalization tank for equalization of flow and its characteristics. An additional facility has been provided at the inlet of equalization tank for pH neutralization. When the equalization tank effluents will be pumped to the pH Adjustment tank where the pH of the effluent is maintained in-between 7.0 to 8.0 by dosing H₂SO₄ or Caustic solution. After achieving the desired level of the pH, the effluent is routed to Flash Mixing Tank where alum solution is added as a coagulant. It requires hydrogen peroxide solution dosing which ensures the low load of sulphides in effluent. The effluent is then routed to Flocculation Tank where addition of de- oiling Polyelectrolyte helps in breaking the oil – water emulsion and formation of alum flocks.

The effluent from flocculation tank is routed to the dissolved air floatation (DAF) tank. Oil skimmer skims off the oily scum generated in the floating tank top. Sludge settled at the bottom of the tank will be removed on periodically. The oily scum and the bottom sludge are routed to the chemical and oily sludge sump and a provision is also made to route the oily scum to wet slop through wet slop oil sump. Finally, DAF effluent is routed to the aeration tank for biological treatment.





Contaminated Rain Water Treatment System

During wet weather, the contaminated rainwater streams of HPL complex will be received in the surge pond. Floating oil skimmer is provided to remove the free oil layer formed in the surge pond and routed to the wet slop oil sump. Provision is made to send the wastewater from the surge pond to TPI separator as and when required.

Effluent in surge pond is received after passing through Bar Screen & Grit Chamber. The effluent can be routed to equalization tank for processing after passing through TPI-02. If effluent quality is fit for disposal, it can be routed to guard pond via TPI-02.

Sanitary Sewer Treatment System

A dedicated underground sanitary sewer network is provided for entire HPL complex including the captive power plant of HPL Co-generation Ltd. and Nitrogen Plant of M/s Praxair India Pvt. Ltd. Sanitary effluent after collection in various suitable pits, is pumped to Bar screening chambers and then the grit chamber for physical removal of scum and suspended solids. Finally, sewer effluent is pumped to Aeration tank of WWTP for Biological Treatment along with other process effluents.

Biological Treatment System

An integrated biological treatment system has been adopted by HPL for reducing the biodegradable organic content of the effluents. The effluent from the DAF tank is routed to aeration tank operating in extended aeration mode for removal of biodegradable organic matter, resulting in reduction of BOD & COD. Aeration conditions are maintained in the tank by entrapment of the atmospheric air with the help of surface aerators.

The nutrients i.e. urea solution & DAP solution will be dosed at the inlet of aeration tank to provide nitrogen, phosphorus for microorganisms. The overflow from the aeration tank will contain a high concentration of microorganisms. A secondary clarifier helps in separating the microorganism from the liquid streams from the bottom sludge and the over flow is the treated effluent. Then aeration tank effluent is routed under gravity to the clarifier. The clarifier is provided with a sludge scraper, which moves slowly to scrap the bio-solids, which settle at the bottom. The collected sludge is routed to the bio-sludge sump (activated sludge sump).





Bio – sludge sump flow is divided into two streams, one is routed to aeration tank and the other going to a sludge thickener. The excess sludge is sent to the thickened sludge sump and the balance stream is recycled back to the aeration tank to maintain the range. The overflow from the clarifier is the treated effluent, which is routed to the guard pond. Two Guard ponds (effluent holding capacity of approx. 8,180 m³) are provided to take care of all types of functional eventualities of the Waste Water Treatment Plant (WWTP). If the effluent does not meet the norms, it can be routed to equalization tank via surge pond for re-processing.

Co-generation power plant, cooling tower, nitrogen plant and DM water plant effluent will be collected in Cooling Tower Blow Down (CTBD) and DM waste pond. CTBD and DM waste pond overflow which is totally free of any organics or oil is routed to treated effluent sump along with treated effluent from guard pond for final disposal through a channel.

Effluent from LLDPE, PP, BDEU and PGHU units are received in receiving sump tank from where overflow of the tank is routed to bar screen, grit chamber, surge pond, respectively. Finally, effluent goes to TPI separator for further treatment and there is provision for pumping the effluent directly to the guard pond if effluent quality remains up to the desired level.

Slop Oil Collection System

The slop oil is collected in wet slop oil tank from various units e.g. TPI separators (I and II), equalization tank, floatation tank and surge ponds. Then slop oil is pumped to slop oil tank. The dry slop oil retained in the tank after decantation of water will be disposed as low grade fuel to external agencies. The decanted water from slop oil tank bottom will be routed to receiving sump by gravity.

Sludge Handling System

The oily sludge from the TPI separator and DAF tank are collected in chemical and oily sludge sump from, where it is routed to sludge thickener. The under flow of the sludge thickener is routed to the thickened sludge sump from where it is pumped to the centrifuged. Dewatering Polyelectrolyte is being dosed in centrifuge to achieved better sludge consistency. Periodically sludge will be collected from centrifuge and is shifted to secure on site storage pit. Latter on the accumulated bio-sludge will be incinerated in incinerator.

2.3 TREATED EFFLUENT QUALITY CHECK

SCIENTIFIC RESEARCH LABORATORY has established an Environmental Laboratory inside HPL in WWTP Laboratory as a third independent party to check the quality of effluent daily as per specifications of effluent standards.



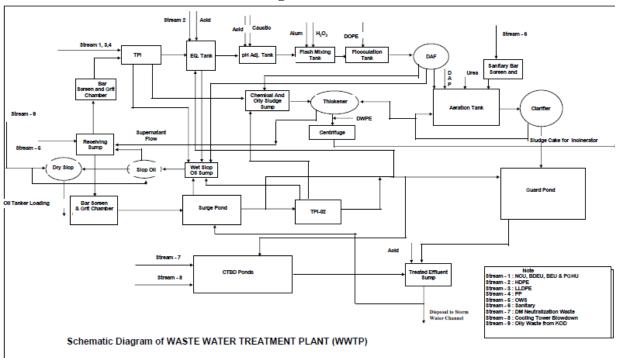


ON-LINE EFFLUENT MONITORING SYSTEM - The On-line effluent monitoring system was installed & successfully commissioned by M/s. Forbes Marshal in Treated Effluent Discharge line for monitoring of flow, pH, TSS, BOD & COD as per the guideline of CPCB. The online data is sent to CPCB/WBPCB server.

2.4 FINAL DISCHARGE SYSTEM

The treated effluent from WWTP will be discharged into the river Hooghly through Green Belt Canal and the treated effluent maximum extent possible will be utilized for irrigation of green belt developments. The final out fall effluents confirm that there is immense dilution i.e. nearly 20,000 times adjacent to the green belt Canal and more than 25,000 times at the confluence of river Haldi. Since Hooghly and Haldi rivers are tidal in nature, the buffering capacity of the green belt canal will be ensured to hold the treated effluent discharged (via green belt canal) during the high tide period. The final effluent is meeting the WBPCB (MINAS) standards.

Flow diagram of WWTP







2.5 METHODS OF MEASUREMENT

Sl. No.	Parameters	Specifiction / Standard (method) or technique used	Range of Testing	Methodology
1.	рН	Standard method (APHA)	0.1-14	pH is determined electrometrically using pH meter provided with pH electrode.
2.	TSS	Filtration Standard Method (APHA)	Min. 0.4 – 1000.0 mg/l	Measured Gravimetrically by filtering through GF/C filter paper.
3.	BOD	BOD Incubator method (APHA)	-	The dissolved oxygen content of the sample with or without dilution is measured before and after incubation at 27°C for 3 days.
4.	COD	Dichromate Reflux Method	-	Sample is refluxed in acid solution with known excess of potassium dichromate. After digestion, the remaining K ₂ Cr ₂ O ₇ is titrated with ferrous ammonium sulphate to determine the amount of K ₂ Cr ₂ O ₇ consumed and the oxidizable organic matter is calculated in terms of oxygen equivalent.
5.	Oil & Grease	Non-dispersive Infrared Analysis Method	0.0-200.0 mg/l	Extracted into Carbon tetrachloride after acidification of the sample and Measured Gravimetrically
6.	Phenol	Chloroform Extraction Method (APHA)	0.001- 0.25mg/l	Steam distilled sample react with 4 – aminoantipyrine in presence of potassium ferricyanide at pH 7.9 and form a coloured antipyrine dye. The dye is extracted from aqueous solution with CHCl ₃ and the absorbance is measured at 460 nm using a UV –VIS spectrophotometer.
7.	Sulphide	Iodometric Method (APHA)	0.1-10.0 mg/l	Iodometric titration with Sodium thiosulphate solution using starch as an indicator.





Sl. No.	Parameters	Specifiction / Standard (method) or technique used	Range of Testing	Methodology
8.	Fluoride	SPADNS Method (APHA)	0.0-1.4 mg/l	Sample mixed with Zirconyl - SPADNS solution and the concentration was measured by the UV-VIS recording spectrophotometer
9.	Cyanide	Colorimetric Method (APHA)	0.02-0.2 mg/l	The alkaline distilled of cyanide is measured by pyridine – barbituric acid reagent using an UV –VIS spectrophotometer
10.	Chromium (cr ⁺⁶)	Colorimetric Method (APHA)	0.01-1.0 mg/l	Determined colorimetrically by reaction with di-phenyl carbazide in acidic solution using spectrophotometer
11.	Total Chromium	Colorimetric Method (APHA)	0.01-1.0 mg/l	Sample is oxidized with potassium permanganate and determined colorimetrically by reaction with diphenyl carbazide in acidic solution spectrophotometer.
12.	Total Iron	Phenanthroline Method (APHA)	0.05-10.0 mg/l	Iron is reduced to ferrous state by Hydroxyl amine hydrochloride and treated with 1,10-phenanthroline at pH 3.2 to 3.3 and measured spectrophotometrically
13.	Total Zinc	Atomic Absorption Spectrophotometeri c Method (APHA)	0.005-2.0 mg/l	Zinc is determined by atomic absorption spectrophotometer using air-acetylene flame
14.	Total Copper	Atomic Absorption Spectrophotometric Method (APHA)	0.01-10.0 mg/l	Copper is determined by atomic absorption spectrophotometer using airacetylene flame
15.	Phosphate (as P)	Stannous Chloride Method (APHA)	0.003-1.0 mg/l	Ammonium molybdate reacts with water sample to form Molybdophosphoric acid and reduced by stannous chloride to intensely coloured molybdenum blue and measured spectrophotometrically.





2.6 WATER CONSUMPTION AND EFFLUENT DISCHARGE

SI. No.	Water Consumption	Average Data of October 2023 to March 2024 (KL/Day)	Conditions as per WBPCB's CTOs (700 KTA Ethylene + Coal Fired Boiler + AdPer Ma (butene – 1 Plant) (KL/Day)
1	Industrial cooling + Boiler feed water + Fire water makeup	34360	49203
2	Domestic purpose	1075	1510
3	Processing where by water gets polluted and the pollutants are easily biodegradable	1777	2000
4	*Total Discharge of Effluent (a+b)	5153	8619.4
	a. Treated Effluent from Guard Pond & Surge Pond	2947	
	b. Effluent from CTBD & DM Regeneration Pond (as diluents)	2207	

^{*}Total effluent after expansion will be 8625 KL/Day (as per the condition of Environment Clearance dated 20.03.2018)

2.7 EFFLUENT QUALITY

Half Yearly Average Data of WWTP Outlet Period of Monitoring: October 2023 to March 2024

Sl.		,	G. I I	WWTP
No.	Parameter	Unit	Standards	Outlet
1.	рН		6.5-8.5	7.53
2.	TSS	mg/l	100	16.39
3.	BOD	mg/l	30	8.69
4.	COD	mg/l	250	42.36
5.	Total Oil &Grease	mg/l	10	< 5.0
6.	Phenol	mg/l	1	< 0.002
7.	Sulphide	mg/l	2	< 0.5
8.	Cyanide	mg/l	0.2	< 0.02
9.	Fluoride	mg/l	5	0.69
10.	Total Chromium	mg/l	2	< 0.05
11.	Chromium (Cr ⁺⁶)	mg/l	0.1	< 0.01
12.	FRC	mg/l	0.5	< 0.1
13.	Temperature	°C	Not>10°C higher than intake	26.0
14.	Iron as Fe	mg/l	1.0	0.33
15.	Zinc as Zn	mg/l	1.0	0.044
16.	Copper as Cu	mg/l	1.0	< 0.05
17.	Phosphate as P	mg/l	5.0	0.925

Note: Intake Temperature 25.5°C





Monthly Average Data of WWTP Outlet

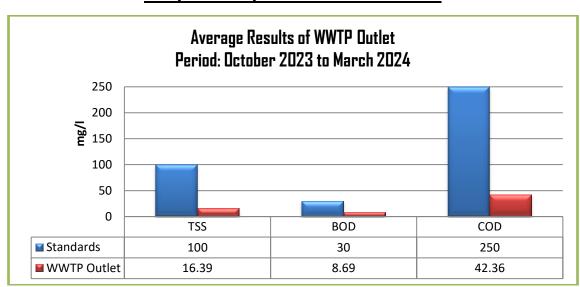
Cl Ma	Donomoton			WWTF	Outlet		
Sl.No.	Parameter	Oct'23	Nov'23	Dec'23	Jan'24	Feb'24	Mar'24
1.	рН	7.72	7.58	7.50	7.42	7.34	7.62
2.	TSS	16.11	16.18	16.50	17.33	16.21	16.03
3.	BOD	9.48	9.23	8.68	8.89	7.72	8.16
4.	COD	46.11	46.0	42.74	42.49	36.79	40.03
5.	Oil & Grease	< 5.0	< 5.0	< 5.0	< 5.0	< 5.0	< 5.0
6.	Phenol	< 0.002	< 0.002	< 0.002	< 0.002	< 0.002	< 0.002
7.	Sulphide	< 0.5	< 0.5	< 0.5	< 0.5	< 0.5	< 0.5
8.	Cyanide	< 0.02	< 0.02	< 0.02	< 0.02	< 0.02	< 0.02
9.	Fluoride	0.67	0.71	0.69	0.70	0.69	0.69
10.	Total Chromium	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05
11.	Chromium (Cr ⁺⁶)	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01
12.	FRC	< 0.1	< 0.1	< 0.1	< 0.1	< 0.1	< 0.1
13.	Temperature	30.0	30.0	25.0	22.0	21.5	27.5
14.	Iron as Fe	0.28	0.31	0.37	0.54	0.13	0.35
15.	Zinc as Zn	0.044	0.035	0.048	0.016	0.075	0.046
16.	Copper as Cu	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05
17.	Phosphate as P	1.72	1.72	1.08	0.22	0.32	0.49

Note: 1) All values are in mg/l except pH & Temperature.

2) Frequency of monitoring a) Sl. No. 1 – 11 & 14 : Daily

b) Sl. No. 12 & 13 : Weekly c) Sl. No. 15 – 17 : Monthly

Graphical Representation of Effluent







WWTP INLET

Sl.	Donomoton	Unit	WWTP Intlet					
No.	Parameter	Unit	Oct'23	Nov'23	Dec'23	Jan'24	Feb'24	Mar'24
1.	pН		9.44	10.22	8.91	9.11	9.35	10.89
2.	Total Suspended Solids	mg/l	34.0	71.00	44.0	74.0	95.0	58.00
3.	Chemical Oxygen Demand	mg/l	279.0	261.00	238.96	220.0	138.0	256.00
4.	Biochemical Oxygen Demand (3 days at 27°C)	mg/l	56.0	61.00	57.0	52.0	36.0	62.00
5.	Oil and Grease	mg/l	< 5.0	< 5.0	< 5.0	< 5.0	< 5.0	< 5.0
6.	Phenol	mg/l	1.18	1.48	1.21	1.35	0.94	1.09
7.	Sulphide (as S)	mg/l	4.74	3.29	3.49	3.23	3.76	3.29
8.	Cyanide (as CN),	mg/l	< 0.02	< 0.02	< 0.02	< 0.02	< 0.02	< 0.02
9.	Fluoride (as F)	mg/l	0.56	0.87	0.73	0.83	0.89	0.88
10.	Total Chromium (as Cr)	mg/l	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05
11.	Hexavalent Chromium (as Cr ⁶⁺)	mg/l	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01
12.	Iron as Fe	mg/l	0.62	0.87	0.51	0.70	0.25	0.77
13.	Zinc as Zn	mg/l	0.085	0.071	0.049	0.047	0.201	0.131
14.	Copper as Cu	mg/l	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05	< 0.05
15.	Phosphate as P	mg/l	0.40	2.11	0.96	0.15	0.42	0.15

Frequency of monitoring
a) Sl. No. 1, 3 & 5 : Daily
b) Others : Monthly

CHAPTER NO. - 03

GASEOUS EMISSION

(STACK MONITORING)





Online Stack Monitoring System at CPP Online SOx, NOx & CO analyser





Online Stack Monitoring System at CFB



Online PM analyser (CPP)







3.0 GASEOUS EMISSION

	GENERAL INFORMATION ABOUT STACK									
SI. No.	Particulars	CFB	Auxiliary Boiler (2 Nos.)	GT & HRSG (2 Nos.)	PGHU	PGDS	*NCU (9 Nos.)	EDG		
1	Stack height from ground level	140.00 mt.	54.3 mt.	45 mt.	33 mt.	30 mt.	40 mt.	17.2 mt.		
2	Sampling port from ground level	81.50 mt.	36.5 mt.	30.5 mt.	24.95 mt.	19.70 mt.		16.4		
3	Stack made by	Concrete	MS	MS	MS	MS	MS	MS		
4	Diameter of the stack at sampling point	7.21 mt.	2.3 mt.	3.6 mt.	0.95 mt.	1.06 mt.	2.1 mt.			
5	Shape of the stack	Circular	Circular	Circular	Circular	Circular		Circular		
6	Area of the stack		4.1527 m ²	10.17 m ²	0.7091 m ²	0.883 m ²		0.0707 m ²		
7	Whether stack is attached with permanent ladder & platform	Yes	Yes	Yes	Yes	Yes	Yes	Yes		
8	Type of Fuel	Coal	CBFS, RFG & Naphtha	Naphtha & RFG	RFG	RFG	RFG	HSD		
9	Fuel consumption (Rated)	3 x 24.07 t/hr.	9.4 TPH (Naphtha)	13.5 TPH(Naphtha)	120 Kg/hr	1.44 KTA (0.16T/Hr.)	2F-201 – 1440 & 2F-202 to 2F- 209 – 3202 T/Month	0.8 KI/hr		
10	Capacity (Rated)	3 x 120 TPH	120 TPH	GT-34.5 MW; HRSG-120 TPH SHP & 22 TPH MP	60 TPH	30 TPH	2F-201 – 13.50 & 2F-202 to 2F- 209 – 32.00 T/Hrs.	1500 KVA		
12	Whether stack is attached with emission control device	Bag Filter, ESP	No	No	No	No	No	NO		

^{*}CPCB Emission Regulations Part-Three for stack is not applicable for NCU. The Licensor did not provide any provision for Iso-Kinetic sampling of flue gas for measurement of PM. However, gas sampling can be done for SO₂, NOx & CO.





Standards of Stacks

Unit	Standards	SO ₂	NOx	со	Hg	PM
NCU & PGHU		50	350			10
PGDS	Standard as per WBPCB	50	250			05
CPP Stacks			100 ppm of 15% excess O ₂	1% V/V		50
CFB	Standard as per CPCB	100	100	1% V/V	0.03	30

All units are expressed as mg/Nm³

Correction Factor: (a) 3 % O₂ for NCU, PGHU & PGDS, (b) 6% O₂ for CFB

Methodology of Stack Sampling & analysis

Sl. No.	Parameters	Specifiction / Standard (method) or technique used	Range of Testing	Methodology
1.	Particulate matter	Emission Regulations, Part – Three, COINDS/18/1984-85 (chapter 2 & 3)	1 mg/m ³ & above	Sampling using stack kit
2.	Nitrogen Oxides	EPA method-7	2-400 mg/m ³	Absorption in hydrogen peroxide- sulphuric acid solution using EPA flask & spectrophotometric analysis
3.	Sulfur-di-oxide	Emission Regulations, Part – Three, COINDS/18/1984-85 (chapter 4)/EPA method-6	3.4mg- 80,000 mg/m ³	Absorption in hydrogen peroxide solution & titration using Ba-perchlorate
4.	Carbon Monoxide (CO)	IS: 5182 (Part 10): 1999 (First Revision)	0.05 – 200 ppm	Sampling of CO in gas sampling tubes & analysis by Non-dispersive Infrared Absorption Method.
5.	Mercury (Hg)	EPA Method – 29	0.1 μg	Analysis by VGA.





Monitoring Frequency Major source of pollutants from various stacks and parameters monitored are as follows:

Sl. No.	Unit	No.of Stack	Parameters	Frequency of Monitoring
1.	Naphtha Cracker Unit	09	SO ₂ , NO _x , CO	Once in a month
2.	Pyrolysis Gasoline Hydrogenation Unit	01	SO ₂ , NO _x , CO, PM	Once in a month
3.	Py-gas Desulfurisation Unit	01	SO ₂ , NO _x , CO, PM	Once in a month
4.	CFB	01	SO_2 , NO_x , CO , PM	Twice in a month
5.	CPP – Auxiliary Boiler & HRSG	04	SO ₂ , NO _x , CO, PM	Once in a month
6.	CPP – Emergency DG	01	SO ₂ , NO _x , CO, PM	Quarterly

STACK MONITORING RESULTS (October 2023 to March 2024)

A.Naphtha Cracker Unit (NCU)

Half-Yearly Average Results

Transferred to the state of the								
Furnace Heater No.	Temp. (⁰ c)	SO ₂ (mg/Nm ³)	NO _x (mg/Nm ³)	CO (mg/Nm ³)				
2F - 201	142.0	8.75	19.60	2.67				
2F - 202	136.5	10.15	23.08	4.00				
2F - 203	117.0	9.39	22.88	4.17				
2F - 204	156.0	6.95	20.94	3.83				
2F - 205	117.0	8.02	24.42	3.50				
2F - 206	152.0	10.65	24.38	3.60				
2F - 207	130.5	10.09	26.56	3.60				
2F - 208	170.0	11.08	18.44	3.60				
2F - 209	146.5	8.50	22.56	3.60				





Stack Monitoring Results – Location Wise

Si.No.		E	Stack W	onitoring Results – Loca		Dogulta	: /	NI3
October 23	Sl.No.	Furnace	Unit	Month of Monitoring	Temp.			
November 23		Heater No.		0 1 22	1 1			
December 23		-				ļ		
Section Sect		-			†			
Section		2F-201			1	1		_
6 March 24 139.0 10.74 24.27 3.0 1 2F-202 March 24 113.0 9.07 15.00 4.0 1 March 24 160.0 11.22 31.15 4.0 2 October 23 117.0 6.26 27.42 3.0 November 23 117.0 8.60 26.71 4.0 December 23 117.0 11.43 28.39 4.0 January 24 121.0 7.87 18.60 5.0 February 24 112.0 12.21 17.21 5.0 March 24 118.0 9.98 18.92 4.0 November 23 155.0 7.39 20.62 3.0 November 23 155.0 7.39 20.62 3.0 December 23 134.0 5.55 24.24 4.0 January 24 144.0 7.74 22.38 5.0 February 24 156.0 6.05 22.85 4.0 March 24				2		1		
Tebruary 24				-	1	1		
March 24	6			March 24	139.0	10.74	24.27	3.0
March 24 160.0 11.22 31.15 4.0		2F-202		February 24	113.0	9.07	15.00	
November 23		21*-202	_	March 24	160.0	11.22	31.15	
December 23	1			October 23	117.0	6.26	27.42	3.0
Section of the image of the i	2			November 23	117.0	8.60	26.71	4.0
Sanuary 24 121.0 7.87 18.60 5.0	3	2E 202		December 23	117.0	11.43	28.39	4.0
6 March 24 118.0 9.98 18.92 4.0 2 October 23 203.0 4.55 14.28 3.0 November 23 155.0 7.39 20.62 3.0 December 23 134.0 5.55 24.24 4.0 January 24 144.0 7.74 22.38 5.0 February 24 156.0 6.05 22.85 4.0 March 24 143.0 10.42 21.27 4.0 October 23 120.0 5.35 19.50 4.0 November 23 120.0 13.35 27.11 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88<	4	2F-2U3		January 24	121.0	7.87	18.60	5.0
1 NCU October 23 203.0 4.55 14.28 3.0 3 2F-204 December 23 155.0 7.39 20.62 3.0 December 23 134.0 5.55 24.24 4.0 January 24 144.0 7.74 22.38 5.0 February 24 156.0 6.05 22.85 4.0 March 24 143.0 10.42 21.27 4.0 October 23 120.0 5.35 19.50 4.0 November 23 120.0 11.35 27.11 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	5			February 24	112.0	12.21	17.21	5.0
November 23 155.0 7.39 20.62 3.0	6			March 24	118.0	9.98	18.92	4.0
3 2F-204 4 December 23 134.0 5.55 24.24 4.0 5 January 24 144.0 7.74 22.38 5.0 6 February 24 156.0 6.05 22.85 4.0 1 October 23 120.0 5.35 19.50 4.0 November 23 120.0 5.35 19.50 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	1		NCU	October 23	203.0	4.55	14.28	3.0
4 January 24 144.0 7.74 22.38 5.0 5 February 24 156.0 6.05 22.85 4.0 March 24 143.0 10.42 21.27 4.0 1 October 23 120.0 5.35 19.50 4.0 November 23 120.0 11.35 27.11 4.0 March 24 109.0 9.04 24.03 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	2			November 23	155.0	7.39	20.62	3.0
4 January 24 144.0 7.74 22.38 5.0 5 February 24 156.0 6.05 22.85 4.0 1 March 24 143.0 10.42 21.27 4.0 2 October 23 120.0 5.35 19.50 4.0 3 December 23 120.0 11.35 27.11 4.0 4 March 24 109.0 9.04 24.03 3.0 4 October 23 149.0 8.48 24.03 4.0 2 November 23 156.0 9.63 21.21 3.0 3 2F-206 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0	3	25.204		December 23	134.0	5.55	24.24	4.0
5 February 24 156.0 6.05 22.85 4.0 1 March 24 143.0 10.42 21.27 4.0 2 October 23 120.0 5.35 19.50 4.0 November 23 120.0 11.35 27.11 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	4	2F-204		January 24	144.0	7.74	22.38	5.0
6 March 24 143.0 10.42 21.27 4.0 1 October 23 120.0 5.35 19.50 4.0 November 23 120.0 11.35 27.11 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	5			February 24	156.0	6.05	22.85	4.0
1 October 23 120.0 5.35 19.50 4.0 November 23 120.0 11.35 27.11 4.0 December 23 120.0 6.32 27.02 3.0 March 24 109.0 9.04 24.03 3.0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	6			March 24	143.0	10.42		4.0
2 November 23 120.0 11.35 27.11 4.0 3 December 23 120.0 6.32 27.02 3.0 4 March 24 109.0 9.04 24.03 3.0 0 October 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 0 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0	1			October 23	120.0	5.35		4.0
3 December 23 120.0 6.32 27.02 3.0 4 March 24 109.0 9.04 24.03 3.0 0ctober 23 149.0 8.48 24.03 4.0 November 23 156.0 9.63 21.21 3.0 December 23 146.0 13.43 28.88 4.0 January 24 156.0 6.41 21.88 4.0	2	25.205		November 23	†	11.35		4.0
4 March 24 109.0 9.04 24.03 3.0 1 October 23 149.0 8.48 24.03 4.0 2 November 23 156.0 9.63 21.21 3.0 3 2F-206 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0		2F-205		December 23		1		3.0
1 October 23 149.0 8.48 24.03 4.0 2 November 23 156.0 9.63 21.21 3.0 3 2F-206 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0		1			1	1		
2 November 23 156.0 9.63 21.21 3.0 3 2F-206 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0					1	1		
3 2F-206 December 23 146.0 13.43 28.88 4.0 4 January 24 156.0 6.41 21.88 4.0		1				1		
4 January 24 156.0 6.41 21.88 4.0		2F-206				1		
						1		
	5	-		March 24	153.0	15.29	25.88	3.0

All values corrected to 3% Oxygen





Stack Monitoring Results – Location Wise

Sl.No.	Furnace	Unit	g	Temp.	Result	ts in mg/	Nm ³
S1.1VU.	Heater No.	Omt	Date of Monitoring	(⁰ C)	SO_2	NO_x	CO
1			October 23	127.0	5.89	25.70	3.0
2			November 23	128.0	10.35	26.61	4.0
3	2F-207		January 24	124.0	9.07	23.22	3.0
4			February 24	131.0	13.39	25.43	4.0
5			March 24	143.0	11.75	31.85	4.0
1			October 23	172.0	8.02	19.12	3.0
2			November 23	174.0	7.67	18.18	3.0
3	2F-208	NCU	January 24	171.0	17.74	17.13	4.0
4			February 24	168.0	12.10	18.14	3.0
5			March 24	165.0	9.89	19.61	5.0
1			October 23	152.0	4.40	16.20	4.0
2			November 23	145.0	6.37	22.98	3.0
3	2F-209		January 24	144.0	9.95	25.14	4.0
4			February 24	144.0	6.61	22.88	4.0
5			March 24	147.0	15.16	25.62	3.0

All values corrected to 3% Oxygen

B. Pyrolysis Gasoline Hydrogenation Unit (PGHU 4F-101) (October 2023 to March 2024)

Furnace Heater No.	Temp.	SO ₂ (mg/Nm ³)	NO _x (mg/Nm ³)	CO (mg/Nm³)	PM (mg/Nm3)
4F - 101	276.5	13.20	33.01	41.33	3.70

Month Wise Report

	Furnace		_	Temp.	Results in mg/Nm3				
Sl. No.	Heater No.	Unit	Date Of Monitoring	in OC	SO_2	NOx	CO	PM	
1			October 23	275.0	13.80	25.50	32.0	4.14	
3			November 23	271.0	9.48	34.85	32.0	3.65	
4	4F-101	PGHU	December 23	273.0	15.44	42.48	38.0	3.18	
5	4F-101	PGHU	January 24	284.0	17.98	34.47	42.0	3.49	
6			February 24	282.0	12.96	31.73	52.0	3.59	
7			March 24	274.0	9.52	29.04	52.0	4.14	

All values Calculated to 3% O2 dry basis





C. Pyrolysis Gasoline De Sulphurisation Unit (PGDS 4F-201) (October 2023 to March 2024)

Furnace Heater No.	Temp.	SO ₂ (mg/Nm ³)	NO _x (mg/Nm ³)	CO (mg/Nm³)	PM (mg/Nm3)
4F - 201	300.0	17.24	38.63	37.40	4.12

Month Wise Report

Sl. No.	Furnace Heater	Unit	Date Of	Temp.	Res	sults in mg/Nm3		
S1. NO.	No.	Omt	Monitoring	in OC	SO_2	NOx	CO	PM
1			November 23	301.0	10.20	28.88	29.0	2.88
2			December 23	293.0	13.01	36.08	32.0	4.17
3	4F - 201	PGDS	January 24	309.0	27.52	49.06	34.0	3.96
4			February 24	301.0	21.10	34.20	46.0	4.65
5			March 24	298.0	14.35	44.95	46.0	4.93

All values Calculated to 3% O2 dry basis

D. Captive Power Plant

(October 2023 to March 2024)

Furnace /Heater	Temp.	SO ₂	NOx	CO	PM
Name	(^{0}c)	(mg/Nm^3)	(mg/Nm^3)	(mg/Nm^3)	(mg/Nm3)
Auxiliary Boiler #1	147.0	9.90	27.36	4.00	6.53
Auxiliary Boiler #2	149.5	10.24	23.59	5.00	7.64
GT & HRSG #2	192.5	10.65	29.96	5.80	5.05
Emergency DG	117.5	9.16	29.02	37.00	11.06

Month Wise Report

Sl. F. W. N. B. 1983 Temp. Results in mg/Nm3											
Funnaga Haatan Na	Data Of Manitaring	Temp.	R	esults in	mg/Nn	n3					
rumace neater No.	Date Of Monitoring	in OC	SO ₂	NOx	CO	PM					
Auvilianu Dailan #1	February 24	147.0	12.54	28.28	4.0	6.11					
Auxiliary Boller #1	March 24	147.0	7.26	26.43	4.0	6.94					
Auvilianu Dailan #2	January 24	145.0	10.44	19.70	5.0	7.95					
2 Auxiliary Boiler #2	March 24	154.0	10.03	27.48	5.0	7.32					
	October 23	193.0	8.98	27.20	4.0	6.62					
	November 23	195.0	11.93	43.32	6.0	4.15					
GT -1 & HRSG - 2	January 24	193.0	9.35	26.43	7.0	4.64					
	February 24	191.0	10.94	27.28	6.0	5.06					
	March 24	191.0	12.06	25.57	6.0	4.78					
Emanaganay DC	November 23	117.0	8.95	25.34	38.0	13.25					
Efficigency DG	February 24	118.0	9.37	32.69	36.0	8.86					
	Furnace Heater No. Auxiliary Boiler #1 Auxiliary Boiler #2 GT -1 & HRSG - 2 Emergency DG	Auxiliary Boiler #1 Auxiliary Boiler #2 Auxiliary Boiler #1 February 24 March 24 November 23 February 24 November 23 February 24	Auxiliary Boiler #1 Auxiliary Boiler #2 October 23 November 23 February 24 147.0 March 24 154.0 October 23 November 23 February 24 193.0 February 24 191.0 March 24 191.0 November 23 November 23 Indicate of Monttoring in OC Indicate of Monttoring in October 24 I	Furnace Heater No. Date Of Monitoring in OC SO2 Auxiliary Boiler #1 February 24 147.0 12.54 Auxiliary Boiler #2 January 24 147.0 7.26 March 24 154.0 10.03 October 23 193.0 8.98 November 23 195.0 11.93 February 24 191.0 10.94 March 24 191.0 12.06 November 23 117.0 8.95 February 24 118.0 9.37	Furnace Heater No. Date Of Monitoring in OC SO2 NOx Auxiliary Boiler #1 February 24 147.0 12.54 28.28 Auxiliary Boiler #2 January 24 147.0 7.26 26.43 Auxiliary Boiler #2 March 24 154.0 10.04 19.70 March 24 154.0 10.03 27.48 October 23 193.0 8.98 27.20 November 23 195.0 11.93 43.32 February 24 191.0 10.94 27.28 March 24 191.0 12.06 25.57 November 23 117.0 8.95 25.34 February 24 118.0 9.37 32.69	Furnace Heater No. Date Of Monitoring in OC SO2 NOx CO Auxiliary Boiler #1 February 24 147.0 12.54 28.28 4.0 Auxiliary Boiler #2 January 24 147.0 7.26 26.43 4.0 March 24 145.0 10.44 19.70 5.0 March 24 154.0 10.03 27.48 5.0 October 23 193.0 8.98 27.20 4.0 November 23 195.0 11.93 43.32 6.0 February 24 191.0 10.94 27.28 6.0 March 24 191.0 12.06 25.57 6.0 Movember 23 117.0 8.95 25.34 38.0 February 24 118.0 9.37 32.69 36.0					

Page - 25





E. Coal Fired Boiler (CFB)

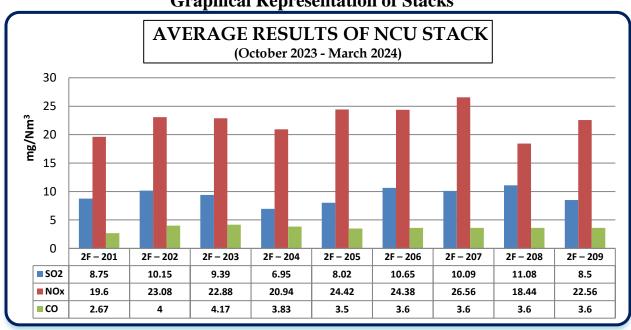
(October 2023 to March 2024)

Temp. (0c)	SO ₂ (mg/Nm ³)	NO _x (mg/Nm ³)	CO (mg/Nm³)	PM (mg/Nm3)
147.0	40.72	60.41	69.17	24.64

Month Wise Report

Sl.	Data Of Manitaring	mg/Nr	ng/Nm3			
No.	Date Of Monitoring	in OC	SO ₂	NOx	CO	PM
1	October 23	149.0	38.98	71.54	74.0	20.67
2		152.0	41.74	57.39	68.0	22.86
3	November 23	152.0	35.67	41.93	66.0	22.58
4		141.0	33.34	51.55	72.0	24.47
5	December 23	143.0	46.21	57.95	69.0	29.41
6	March 23	143.0	48.40	82.09	66.0	27.85

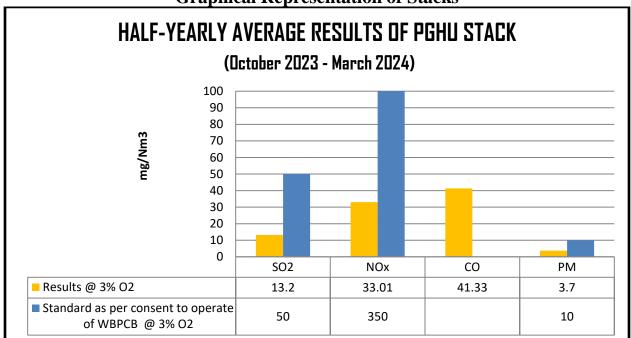
Graphical Representation of Stacks

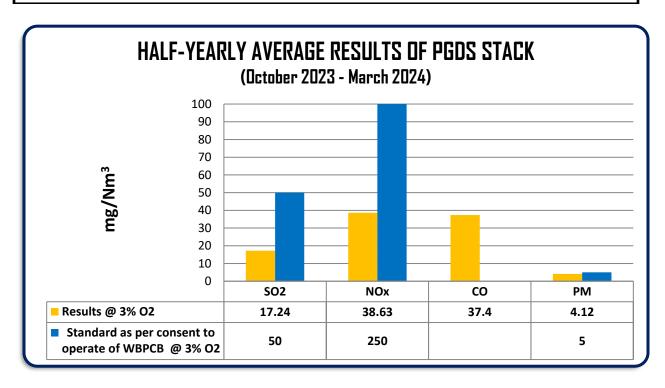






Graphical Representation of Stacks

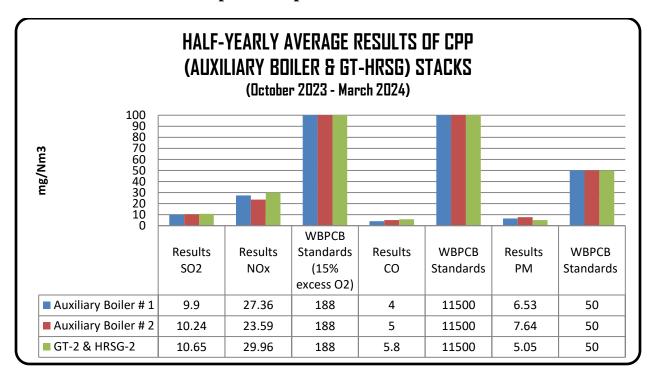


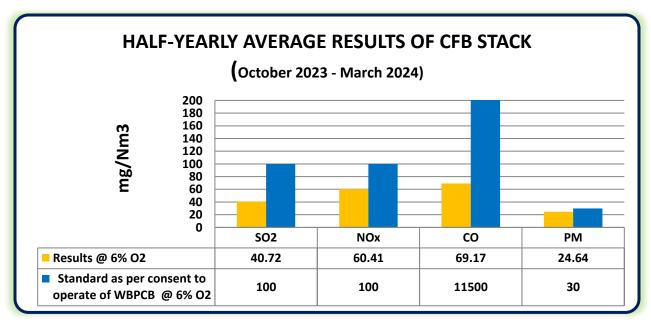






Graphical Representation of Stacks





CHAPTER NO. - 04 METEOROLOGY





4. METEOROLOGY

The following Meteorological parameters:

- > Temperature (Dry & Wet Bulb),
- ➤ Relative Humidity
- Wind Speed And Direction
- > Atmospheric Pressure
- Cloud Cover (Visual Inspection)
- ➤ Rainfall

Following instruments are used for conducting meteorological data recording:

Temperature and relative humidity : Dry & Wet Bulb Thermometer And Sychrometric Chart

Wind direction and wind velocity : Wind - Vane And Cup Counter Anemometer

Rainfall : Rain Gauge Atmospheric Pressure : Barometer

Wind direction was recorded in all the sixteen directions.

A. Abstract of monitored meteorological data (Half-Yearly Max. & Min.):

Location: WWTP (Roof of Environmental Laboratory), HPL Plant Monitoring Period: October 2023 to March 2024.

Monitoring Frequency: Twice in a week

	Velocity n/hr)	Tempe (O ⁰		RH	(%)	Predon Wind D		Rainfall (mm)	Caln	1 (%)
Max.	Min.	Max.	Min.	Max.	Min.	Day	Night		Day	Night
23.7	0.1	39.0	12.0	96.0	30.0	N	NE	313.10	6.02	2.53

B. Abstract of monitored meteorological data (Monthly Max. & Min.):

Month	Wind Velocity (Km/hr)		Temperature (°C)		RH (%)		Predominant Wind Direction		Rainfall (mm)	Calm (%)	
	Max.	Min.	Max.	Min.	Max.	Min.	Day	Night	Monthly	Day	Night
October 2023	23.7	0.5	39.0	25.0	96.0	30.0	NNE	N	172.70	7.69	1.89
November 2023	10.1	0.7	33.5	21.5	96.0	31.0	NNW	N	22.50	6.30	1.06
December -2023	13.9	0.5	30.0	14.5	95.0	43.0	N	NE	6.50	2.10	12.26
January -2024	16.9	0.2	26.0	12.0	94.0	41.0	N	NE	31.40	5.59	10.38
February 2024	15.2	0.1	31.5	15.0	95.0	35.0	SE	ENE	22.20	2.10	5.32
March 2024	18.6	0.7	35.5	21.0	92.0	41.0	ESE	SSE	57.80	0.00	8.49





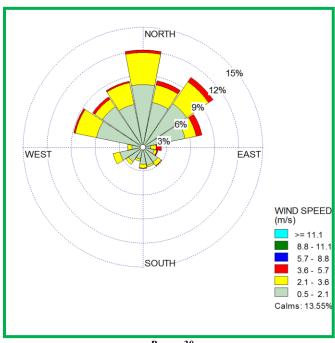
C. Meteorological Observation:

WINDROSE-FREQUENCY TABLE – FULL TIME

(Period: October 2023 to March 2024)

(renou. October 2023 to Watch 2024)											
WIND			VELOCITY	(in m/sec) RA	NGES						
DIRECTION	0.5 <v<=2.1< th=""><th>2.1<v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<></th></v<=2.1<>	2.1 <v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<>	3.6 <v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<>	5.7 <v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<>	8.8 <v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<>	V>=11.1	SUM%				
N	7.82	3.98	0.34	0.00	0.00	0.00	12.14				
NNE	5.74	2.23	0.54	0.00	0.00	0.00	8.51				
NE	6.61	3.31	0.67	0.00	0.00	0.00	10.59				
ENE	5.40	1.42	0.74	0.00	0.00	0.00	7.56				
E	1.01	0.67	0.67	0.00	0.00	0.00	2.35				
ESE	1.48	0.34	0.13	0.00	0.00	0.00	1.95				
SE	2.29	0.54	0.07	0.00	0.00	0.00	2.90				
SSE	2.36	0.20	0.00	0.00	0.00	0.00	2.56				
S	2.16	0.47	0.07	0.00	0.00	0.00	2.70				
SSW	1.55	0.27	0.00	0.00	0.00	0.00	1.82				
SW	2.23	0.41	0.00	0.00	0.00	0.00	2.64				
WSW	2.97	0.88	0.00	0.00	0.00	0.00	3.85				
W	1.42	0.54	0.00	0.00	0.00	0.00	1.96				
WNW	5.94	2.70	0.20	0.00	0.00	0.00	8.84				
NW	6.14	1.15	0.34	0.00	0.00	0.00	7.63				
NNW	5.47	2.77	0.20	0.00	0.00	0.00	8.44				
SUM%	60.59	21.88	3.97	0.00	0.00	0.00	86.44				
CALM		·	(0.00<=V	V <= 0.5)	_		13.56				
	·	·	·	·	_		100.00				

WINDROSE & GRAPH – FULL TIME



Page - 30

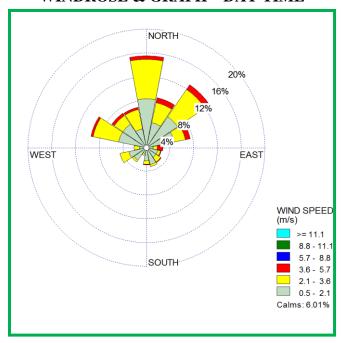




WINDROSE-FREQUENCY TABLE – DAY TIME

WIND		HUDICOL	_	(in m/sec) RA	NGES		
DIRECTION	0.5 <v<=2.1< th=""><th>2.1<v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<></th></v<=2.1<>	2.1 <v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<>	3.6 <v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<>	5.7 <v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<>	8.8 <v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<>	V>=11.1	SUM%
N	8.26	6.61	0.59	0.00	0.00	0.00	15.46
NNE	4.37	3.42	0.83	0.00	0.00	0.00	8.62
NE	6.42	5.55	0.94	0.00	0.00	0.00	12.91
ENE	4.84	1.89	0.83	0.00	0.00	0.00	7.56
E	1.18	0.71	0.94	0.00	0.00	0.00	2.83
ESE	2.00	0.47	0.12	0.00	0.00	0.00	2.59
SE	2.00	0.94	0.12	0.00	0.00	0.00	3.06
SSE	2.95	0.35	0.00	0.00	0.00	0.00	3.30
S	2.24	0.59	0.12	0.00	0.00	0.00	2.95
SSW	1.06	0.35	0.00	0.00	0.00	0.00	1.41
SW	2.60	0.35	0.00	0.00	0.00	0.00	2.95
WSW	3.07	1.53	0.00	0.00	0.00	0.00	4.60
\mathbf{W}	1.30	0.83	0.00	0.00	0.00	0.00	2.13
WNW	4.84	4.37	0.35	0.00	0.00	0.00	9.56
NW	4.84	1.77	0.47	0.00	0.00	0.00	7.08
NNW	3.31	3.31	0.35	0.00	0.00	0.00	6.97
SUM%	55.28	33.04	5.66	0.00	0.00	0.00	93.98
CALM			V=>00.0)	/<= 0.5)			6.02
							100.00

WINDROSE & GRAPH – DAY TIME



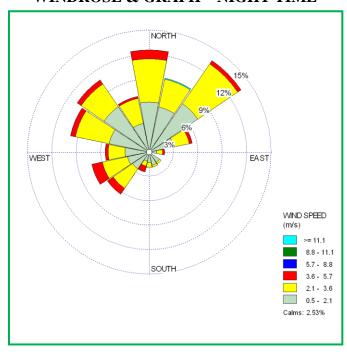




WINDROSE-FREQUENCY TABLE – NIGHT TIME

WIND			VELOCITY	(in m/sec) RA	NGES		
DIRECTION	0.5 <v<=2.1< th=""><th>2.1<v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<></th></v<=2.1<>	2.1 <v<=3.6< th=""><th>3.6<v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<></th></v<=3.6<>	3.6 <v<=5.7< th=""><th>5.7<v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<></th></v<=5.7<>	5.7 <v<=8.8< th=""><th>8.8<v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<></th></v<=8.8<>	8.8 <v<=11.1< th=""><th>V>=11.1</th><th>SUM%</th></v<=11.1<>	V>=11.1	SUM%
N	6.14	5.30	1.08	0.00	0.00	0.00	12.52
NNE	5.66	3.49	0.00	0.00	0.00	0.12	9.27
NE	7.28	5.90	0.48	0.00	0.00	0.00	13.66
ENE	3.13	1.93	0.36	0.00	0.00	0.00	5.42
E	0.96	0.72	0.24	0.00	0.00	0.00	1.92
ESE	0.00	0.00	0.00	0.00	0.00	0.00	0.00
SE	1.57	0.24	0.00	0.00	0.00	0.00	1.81
SSE	1.69	0.24	0.00	0.00	0.00	0.00	1.93
S	1.33	0.60	0.00	0.00	0.00	0.00	1.93
SSW	1.20	0.60	0.72	0.00	0.00	0.00	2.52
SW	2.53	2.89	0.84	0.00	0.00	0.00	6.26
WSW	2.77	3.13	1.33	0.00	0.00	0.00	7.23
W	3.01	2.05	0.36	0.00	0.00	0.00	5.42
WNW	5.06	4.22	0.60	0.00	0.00	0.00	9.88
NW	6.75	3.37	0.60	0.00	0.00	0.00	10.72
NNW	3.61	3.13	0.24	0.00	0.00	0.00	6.98
SUM%	52.69	37.81	6.85	0.00	0.00	0.12	97.47
CALM			(0.00<=V	V<= 0.5)			2.53
						•	100.00

WINDROSE & GRAPH – NIGHT TIME



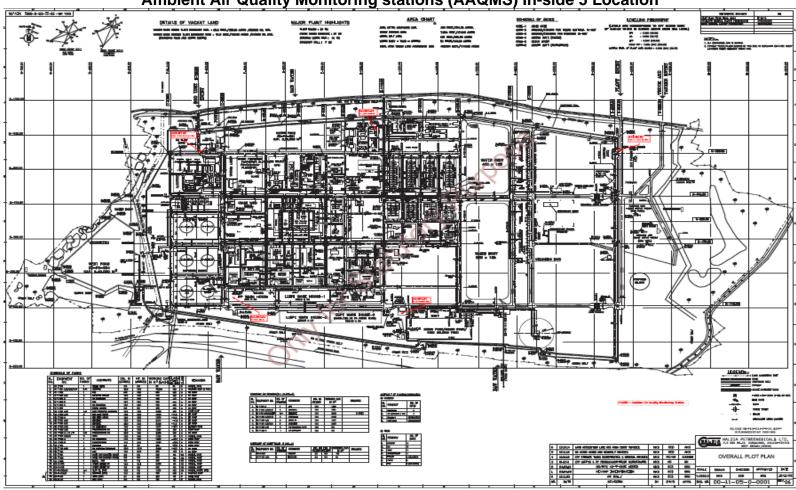
Page-32

CHAPTER NO. - 05

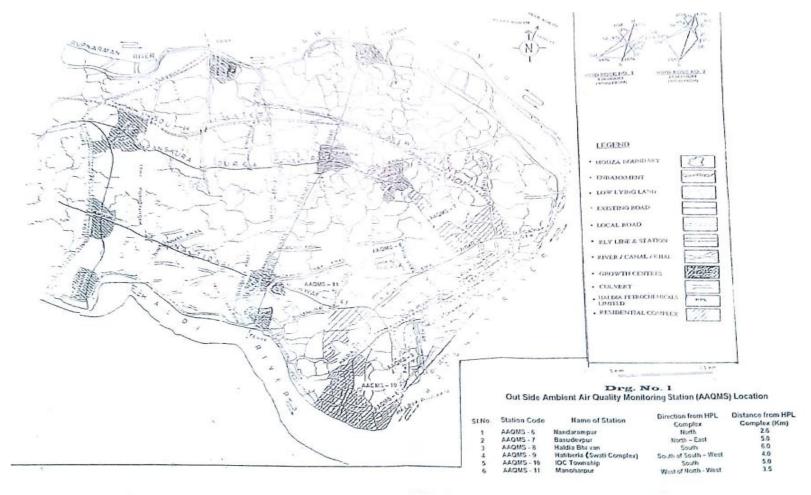
AMBIENT AIR QUALITY

5.0 AMBIENT AIR QUALITY

Ambient Air Quality Monitoring stations (AAQMS) In-side 5 Location



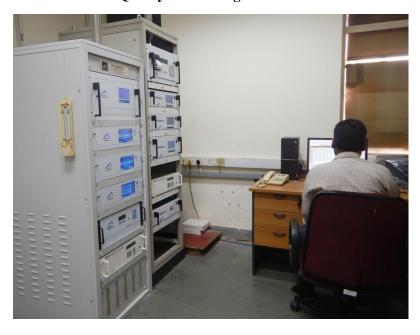
Ambient Air Quality Monitoring stations (AAQMS) Out-side 6 Location







On-Line Ambient Air Quality Monitoring Station at South Control Room



On-Line Hydrocarbon Analyzer at Central Laboratory







Ambient Air Quality Monitoring stations (AAQMS)

A. In Side Ambient Air Quality Monitoring stations (Five locations):

Sl. No.	Station	Station Name	Direction from the center of the plant
	Code		
1	AAQMS - 1	Central Laboratory	North
2	AAQMS - 2	Gate No. 1	East
3	AAQMS - 3	South Control Room	South
4	AAQMS - 4	PP Ware House	South – West
5	AAQMS - 5	CPP Entry Gate	North - West

B. Out Side Ambient Air Quality Monitoring stations (Six locations):

Sl.	Station Code	Name of Station	Direction from HPL	Distance from HPL	
No.			Complex	Complex (km)	
1.	AAQMS – 6	Nandarampur	North	2.6 Km	
2.	AAQMS – 7	Basudevpur	North- East	5.0 Km	
3.	AAQMS - 8	Haldia Bhavan	South	6.0 Km	
4.	AAQMS – 9	Hatiberia (Swati Complex)	South of South-West	4.0 Km	
5.	AAQMS - 10	IOC Township	South	5.0 Km	
6.	AAQMS – 11	Manaharpur	West of North-West	3.5 Km	

C. Methodology of Ambient Air Sampling & Analysis

	C. Methodology of Ambient Air Sampling & Analysis										
Sl.	Parameters	Unit	Specifiction /	Range of	Methodology						
No.			Standard (method)	Testing							
			or technique used								
1	Particulate	$\mu g/m^3$	IS: 5182(Part 23):	$1 \mu g/m^3 \&$	Sampling of PM ₁₀ using						
	Matter (PM ₁₀)		2006	above	Respirable Dust Sampler						
2	Particulate	$\mu g/m^3$	USEPA 40 CFR	$2 \mu g/m^3 \&$	Sampling of PM _{2.5} using						
	Matter (PM _{2.5})		Parts 53 & 58	above	Ambient Fine Dust Sampler,						
3	Sulphur	$\mu g/m^3$	IS:5182 (Part-	$4 \mu g / m^3 \&$	Absorption in Na-						
	Dioxide (SO ₂)		2):2006 (First	above	tetrachloromercurate solution						
			Revision)		followed by						
					Spectrophotometric analysis						
4	Oxides of	$\mu g/m^3$	IS:5182 (Part-	$10 \mu g / m^3 \&$	Absorption in sodium						
	Nitrogen (NO _x)		6):2006 (First	above	hydroxide & Na-arsenite						
			Revision)		solution followed by						
					Spectrophotometric analysis						





Sl.	Parameters	Unit	Specifiction /	Range of	Methodology
No.			Standard (method)	Testing	
		. 2	or technique used	2.5	
5	Ozone (O ₃)	$\mu g/m^3$	Methods of air	$8.2 \mu g / m^3 \&$	Micro-amounts of O ₃ liberate
			sampling and	above	iodine when absorbed in a 1%
			examination, Third		solution of potassium iodide
			Edition, Edited by		buffered at pH $6.8(\pm 0.2)$. The liberated iodine is determined
			James P. Lodge, Method 411.		Spectrophotometrically by
			Michiou 411.		measuring the absorption of
					triiodide ion at 352 nm.
6	Ammonia	μg/m ³	Method of Air	$5 \mu g / m^3 \&$	Ammonia is absorb in dilute
	(NH_3)	, 0	Sampling &	above	H ₂ SO4 & measured
			examination, Third		colorimetrically by reaction
			Edition, Edited by		with phenol & alkaline
			James P. Lodge,		sodium hypochlorite to
			Method 401		produce indophenols, a blue
7	Lood (Db)		Mathad of Air	0.01	dye.
7	Lead (Pb)	$\mu g/m^3$	Method of Air Sampling &	$0.01 \mu g$ /m ³ & above	Lead is determined by Atomic Absorption
			examination, Third	/III & above	Spectrophotometer using air-
			Edition, Edited by		acetylene flame.
			James P. Lodge,		decty ione name.
			Method 303A, 822		
8	Benzene (C ₆ H ₆)	$\mu g/m^3$	IS: 5182(Part 11):	0.042 μg	Absorption on activated
			2006	/m ³ & above	charcoal, desorption by carbon
					disulphide & analysis by GC
		, 3	G 1 136 1 1	0.14 / 3.0	using FID.
9	Arsenic (As)	ng/m ³	Standard Method-	$0.14 \text{ ng/m}^3 \&$	Standard Method-APHA, 20 th
			APHA, 20 th Edition,	above	Edition, 1998 by Atomic Absorption
					Spectrophotometer using
					vapour generation assembly
					(VGA)
10	Nickel (Ni)	ng/m ³	Method of Air	$2.8 \text{ ng/m}^3\&$	Nickel is determined by
			Sampling &	above	Atomic Absorption
			examination, Third		Spectrophotometer using air-
			Edition, Edited by		acetylene flame
			James P. Lodge,		
			Method 303A, 822		





Sl. No.	Parameters	Unit	Specifiction / Standard (method) or technique used	Range of Testing	Methodology
11	Benzo (a)	ng/m ³	IS: 5182(Part 12):	$0.11 \text{ ng/m}^3 \&$	Benzo(a)pyrene and other
	Pyrene (BaP),		2009	above	polynuclear hydrocarbons are
	Particulate				extracted from the particulate
	phase only				matter using a non-polar
					solvent cyclohexane, which
					extracts less extraneous
					material than a more polar
					solvent. The extract is
					concentrated and analyzed by
					Gas Chromatograph – Mass
					Spectrometer.
12	Carbon	mg/m ³	IS: 5182 (Part	0.01 mg	Sampling of CO in gas
	Monoxide		10): 1999 (First	/m ³ & above	sampling tubes & analysis by
	(CO)		Revision)		NDIR

D. National Ambient Air Quality Standards

Sl.	Parameters		Time	Ambient air conce	entration (µg/m³)
No.		Unit	Weighted	Industrial,	Ecologically
			Average	Residential, Rural	Sensitive Area
				& Other Area	
1	Sulphur Dioxide (SO ₂)	$\mu g/m^3$	Annual*	50	20
			24 hours**	80	80
2	Nitrogen Dioxide (NO ₂)		Annual*	40	30
			24 hours**	80	80
3	Particulate Matter		Annual*	60	60
	(PM_{10})		24 hours**	100	100
4	Particulate Matter		Annual*	40	40
	$(PM_{2.5})$		24 hours**	60	60
5	Ozone (O ₃)		8 hours**	100	100
			1 hours**	180	180
6	Lead (pb)		Annual*	0.50	0.50
			24 hours**	1.0	1.0
7	Carbon monoxide (CO)	mg/m^3	8 hours**	02	02
			1 hours**	04	04





Sl.	Parameters		Time	Ambient air conce	entration (µg/m³)
No.		Unit	Weighted Average	Industrial, Residential, Rural & Other Area	Ecologically Sensitive Area
8	Ammonia (NH ₃)	μg/m ³	Annual*	100	100
			24 hours**	400	400
9	Benzene (C ₆ H ₆)		Annual*	05	05
10	Benzo(a)Pyrene (BaP)	ng/m ³	Annual*	01	01
11	Arsenic (As)		Annual*	06	06
12	Nickel (Ni)		Annual*	20	20

^{*} Annual arithmetic mean of minimum 104 measurements in a year at a particular site taken twice a week 24 hourly at uniform intervals.

Note.-Whenever and wherever monitoring v results on two consecutive days of monitoring exceed the limits specified above for the respective category, it shall be considered adequate reason to institute regular or continuous monitoring and further investigation.

^{** 24} hourly or 08 hourly monitored values, as applicable, shall be complied with 98% of the time in a year. 2% of the time, they may exceed the limits but not on two consecutive days of monitoring.





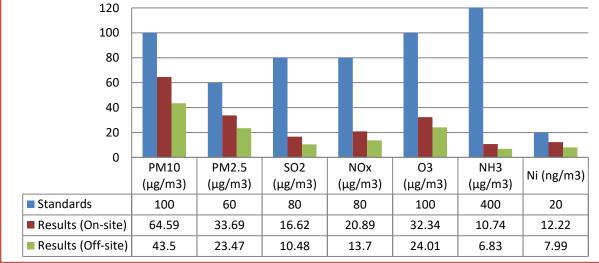
MONTHLY AVERAGE RESULTS OF AMBIENT AIR QUALITY (On-site Plant)

Month	PM ₁₀	PM _{2.5}	SO ₂	NOx	C ₆ H ₆	CO	O_3	NH ₃	BaP	As	Ni	Pb
Month	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	(mg/m^3)	$(\mu g/m^3)$	$(\mu g/m^3)$	(ng/m^3)	(ng/m^3)	(ng/m ³⁾	$(\mu g/m^3)$
Oct 23	49.53	25.17	15.13	19.74	1.63	0.543	31.14	9.91	0.07	4.45	12.39	0.144
Nov 23	54.19	28.25	16.46	21.51	1.81	0.562	32.31	11.10	0.18	4.35	12.15	0.141
Dec 23	65.37	34.44	16.70	21.21	2.23	0.564	30.70	11.09	0.33	4.47	12.41	0.146
Jan 24	73.57	36.83	17.54	20.70	2.51	0.569	30.86	10.99	0.39	4.22	12.13	0.138
Feb 24	70.23	39.82	17.32	20.98	2.74	0.667	33.91	10.72	0.40	4.28	12.10	0.136
Mar 24	74.66	37.65	16.55	21.17	2.79	0.566	35.13	10.64	0.42	4.22	12.13	0.138
Average	64.59	33.69	16.62	20.89	2.29	0.58	32.34	10.74	0.30	4.33	12.22	0.140

MONTHLY AVERAGE RESULTS OF AMBIENT AIR QUALITY (Off-site Plant)

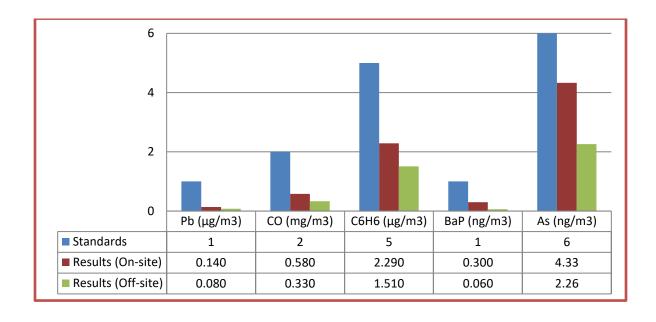
								& 0.12=2.	(3100 1 10011	- /	
Month	PM_{10}	PM _{2.5}	SO_2	NOx	C_6H_6	CO	O_3	NH_3	BaP	As	Ni	Pb
Monui	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	$(\mu g/m^3)$	(mg/m^3)	$(\mu g/m^3)$	$(\mu g/m^3)$	(ng/m^3)	(ng/m^3)	(ng/m^3)	$(\mu g/m^3)$
Oct 23	35.16	19.16	11.05	14.49	1.14	0.339	23.00	6.25	0.05	2.27	8.10	0.077
Nov 23	40.65	21.51	10.51	13.83	1.44	0.321	23.74	6.63	0.05	2.33	7.68	0.078
Dec 23	46.58	24.14	10.37	14.08	1.69	0.375	22.98	7.39	0.05	2.22	7.84	0.076
Jan 24	49.42	26.29	10.75	13.10	1.68	0.386	24.16	7.00	0.09	2.26	8.05	0.083
Feb 24	44.43	24.21	10.39	12.58	1.56	0.318	25.16	6.73	0.05	2.24	8.19	0.084
Mar 24	44.75	25.50	9.81	14.12	1.52	0.260	25.02	6.97	0.07	2.26	8.05	0.083
Average	43.50	23.47	10.48	13.70	1.51	0.33	24.01	6.83	0.06	2.26	7.99	0.080

Graphical Representation of AAQ Data









CHAPTER NO. - 06

VENT EMISSION & WORK ZONE & IR QUALITY





6.0 VENT EMISSION AND WORK ZONE AIR QUALITY

A. Methods of measurement

Sl.	Parameters	Parameters Standards of measurement		Methodology
No.			Testing	
1.	Benzene	Method no. 12, OSHA	0.04 ppm	Absorption on activated charcoal,
			& above	desorption by carbon disulphide &
				analysis by GC using FID
2.	Butadiene	Method no. 56, OSHA	0.09 ppm	Absorption on activated charcoal,
			& above	desorption by carbon disulphide &
				analysis by GC using FID
3.	Hexane	Methods of Air Sampling and	0.05 ppm	Absorption on activated charcoal,
		Examination, Third Edition. Edited by	& above	desorption by carbon disulphide &
		James P. Lodge, Method 109		analysis by GC using FID

Work Zone Monitoring Results <u>Half-Yearly Average Results</u> (October 2023 to March 2024)

(
Plant	Standard (ppm)	Average Results (ppm)				
Benzene Extraction Unit	1.0	0.153				
Butadiene Extraction Unit	1.0	0.231				
Hexane Area	500.0	10.37				

Standards as per OSHA (TWA for 8 hrs. exposure)

Month-Wise Results

(October 2023 to March 2024)

	BI	ENZENE	BUTA	DIENE	HEXANE	
Month	5P – 02 A & B Hartcut Feed Pump(BEU)	Benzene Sampling Point (050-SP- 108)& 5P-07 A & B (BEU)	In Front Of Vessel No581	Butadiene product sampling point	V- 2405 Draining Point	Flaker House(Ground Floor)
Oct 23	0.053	0.206	0.128	0.257	7.96	11.21
Nov 23	0.059	0.217	0.137	0.289	8.39	11.36
Dec 23	0.068	0.232	0.153	0.302	8.78	11.84
Jan 24	0.077	0.256	0.168	0.325	9.43	12.71
Feb 24	0.064	0.224	0.148	0.296	8.64	10.86
Mar 24	0.089	0.286	0.197	0.373	9.95	13.27

All results are in ppm.

Month-Wise Benzene Emission from Vent of Benzene Extraction Unit & Benzene Recovery Unit. (October 2023 to March 2024)

Location	Standard	Month
BEU	5.0 mg/l	All results are well below the standards in all months (<0.1mg/l)

CHAPTER NO. - 07

AMBIENT NOISE





7.0 AMBIENT NOISE

In order to establish ambient noise levels for the Study Area, measurement of noise levels were performed at seven locations. i.e 5 (Five) Nos. of identified main noise generation units and 5 (Five) locations at the boundary wall (1 meter away from the boundary walls). Noise monitoring was measured in decibel unit i.e. Leq dB(A) where A denotes the frequency weighting in the measurement of noise and corresponds to frequency response characteristics of the human ear and Leq is an energy mean of the noise level, over a specified period. Monitoring was carried out once in a season in each location.

The monitoring locations in plant boundary for ambient noise level are as follows:

Sl.No.	Location Details	Location Code	Direction from the plant Center
1.	Near Gate No1	AN 1	East of north east
2.	Near Gate No3	AN 2	East of south east
3.	South Gate	AN 3	South
4.	CPP	AN4	North of north west
5.	North Gate	AN5	North

24 hours Noise (Ambient Noise) Standards (CPCB & WBPCB Standards)

Dunation	Unit are dB(A)				
Duration	Industial	Commercial	Residential	Silence	
DAY (6 am to 10 pm)	75	65	55	50	
NIGHT (10 pm to 6 am)	70	55	45	40	

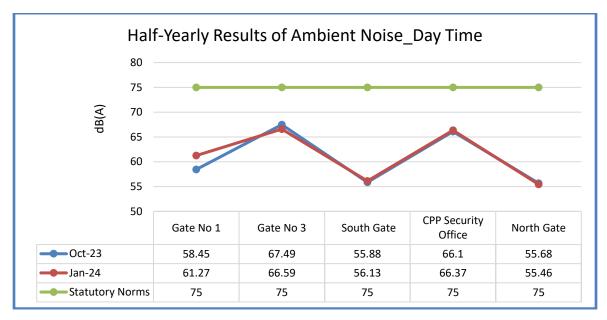
Ambient Noise Level (Average) Apr 2023 to Sept 2023

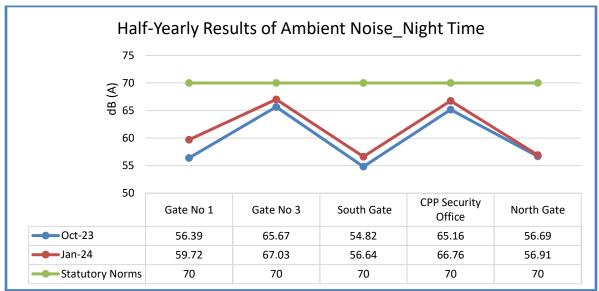
LOCATION	Octob	oer 2023	January 2024	
LOCATION	Day	Night	Day	Night
Near Gate No-1	58.45	56.39	61.27	59.72
Near Gate No-3	67.49	65.67	66.59	67.03
Near South Gate	55.88	54.82	56.13	56.64
Near CPP Security Office	66.10	65.16	66.37	66.76
Near North Gate	55.68	56.69	55.46	56.91





Graphical Representation of Ambient Noise Data





CHAPTER NO. - 08 LEAK DETECTION UNDER LDAR PROGRAM





8.0 LDAR PROGRAM

Fugitive emission monitoring

Fugitive Emission Sources:

Fugitive emission sources include leaks of hydrocarbon vapors from process equipment and evaporation of hydrocarbons from open areas, rather than through a stack or vent. Fugitive emission sources include valves of all types, flanges, pump seals, process drains, cooling towers, and oil/water separators. Normally, control of fugitive emissions involves minimizing leaks and spills through equipment changes, procedure changes, and improved monitoring, housekeeping, and maintenance practices.

Fugitive emission monitoring:

The technique which has been used to detect and control emissions from equipment leaks is known as Leak Detection and Repair (LDAR) Programme. The method which is used in LDAR program is Stratified Emission Factor Method. In this method the screening values are distributed in different ranges, like

- 0-1000 ppmv
- 1001-10,000 ppmv
- Over 10,000 ppmv

Emission factors for each screening value range have been generated from data gathered during previous EPA studies. These stratified emission factors represent the leak rate measured during fugitive emission testing. Their development incorporated the statistical methods used by EPA in developing other emission factors. The emission factor for each discrete interval, by equipment type and service, is presented in the table.

Emiss	sion Factors(kg/hr	/source) for Scree	ning value range (p	opmv)
Source	Service	0-1000	1001-10000	Over- 100000
Valves	Gas/Vapor	0.00014	0.00165	0.0451
	Light liquid	0.00028	0.00963	0.0852
	Heavy liquid	0.00023	0.00023	0.00023
Pump	Light liquid	0.00198	0.0335	0.437
	Heavy liquid	0.0038	0.0926	0.3885
Compressor	Gas/Vapor	0.01132	0.264	1.608
seals				
Pressure relief	Gas/Vapor	0.0114	0.279	1.691
devices				
Source	Service	0-1000	1001-10000	Over- 100000
Flanges,	All	0.00002	0.00875	0.0375
connections				
Open-ended	All	0.00013	0.00876	0.01195
lines				





Reference: USEPA Handbook on Control Techniques for Fugitive VOC Emissions from Chemical Process Facilities. EPA/625/R-93/005, March 1994.

All screening values must be recorded according to the applicable ranges. The product of the appropriate emission factor and the number of components in each screening value range and source type. The total emission rate is the sum of all the emission rates for each value range and source type.

EE=(NL1*SEF1)+(NL2*SEF2)+(NL3*SEF3)
EE=emission estimate
NL1= number leaking in first range (0-1000)
NL2= number of leaking in second range (1001-10,000)
NL3= number of leaking component in third range(over 10,000)
SEF1= stratified emission factor for first range
SEF2= stratified emission factor for second range
SEF3= stratified emission factor for third range

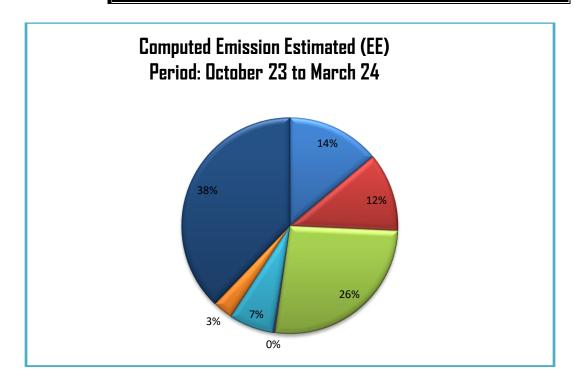
LDAR program has been adopted for identifying the leakage valves, pumps and flanges and quantifying the total VOC emitted from those equipments of different units. The points where the emission is over 1 ppm are considered as leaking points. Based on those identified points the total VOC emission will be estimated for each unit.

Total VOC emission from NCAU (BDEU, BEU, PGHU, PGDS, Butene-1 & CHU), NCU

Location	Computed Emission Estimates (EE) Actual Unit – Ton/Annum	Computed Emission Estimates (EE) in 100%
BDEU	0.075	13.98
BEU	0.063	11.74
PGHU	0.142	26.46
PGDS	0.0016	0.30
BUTENE-1	0.036	6.71
CHU	0.016	2.98
NCU	0.203	37.83
Total	0.537	100.00







Total VOC emission from NCAU (BDEU, BEU, PGHU, PGDS, Butene-1 & CHU), NCU

1. Total VOC emission from BDEU measured in November 23:

No of points checked: 747

No of leaking (VOC>1ppm) points: 75

No of non leaking points: 672

	Number of S	ource Scree	Computed Emission Estimates (EE)		
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dryman	Light liquid	1	0	0	0.00198
Pump	Heavy liquid	0	0	0	0
	Gas/Vapor	0	0	0	0
Valve	Light liquid	20	0	0	0.0056
	Heavy liquid	0	0	0	0
Flange	All	54	0	0	0.00108
				Total	0.00866
					6.23(kg/month) / 0.075 (Ton/Annum)





2. Total VOC emission from BEU measured in December 23:

No of points checked: 726

No of leaking (VOC>1ppm) points: 70

No of non leaking points: 656

	Number of So	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dump	Light liquid	1	0	0	0.00198
Pump	Heavy liquid	0	0	0	0
	Gas/Vapor	0	0	0	0
Valve	Light liquid	15	0	0	0.0042
	Heavy liquid	0	0	0	0
Flange	All	54	0	0	0.00108
				Total	0.00726
					5.23(kg/month) / 0.063 (Ton/Annum)

3. Total VOC emission from PGHU measured in January 24:

No of points checked: 936

No of leaking (VOC>1ppm) points: 124

No of non leaking points: 812

	Number of S	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Duman	Light liquid	3	0	0	0.00594
Pump	Heavy liquid	0	0	0	0
Valve	Gas/Vapor	2	0	0	0.00028
	Light liquid	30	0	0	0.0084
	Heavy liquid	0	0	0	0
Flange	All	89	0	0	0.00178
				Total	0.0164
					11.81 (kg/month) / 0.142 (Ton/Annum)

4. Total VOC emission from PGDS measured in February 24:

No of points checked: 135

No of leaking (VOC>1ppm) points: 9 No of non leaking points: 126

	Number of So	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dryman	Light liquid	0	0	0	0
Pump	Heavy liquid	0	0	0	0
Valve	Gas/Vapor	0	0	0	0
	Light liquid	0	0	0	0
	Heavy liquid	0	0	0	0
Flange	All	9	0	0	0.00018
				Total	0.00018
					0.13 (kg/month) / 0.0016 (Ton/Annum)





5. Total VOC emission from Butene -1 measured in February 24:

No of points checked: 636

No of leaking (VOC>1ppm) points: 90

No of non leaking points: 546

	Number of S	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dryman	Light liquid	0	0	0	0
Pump	Heavy liquid	0	0	0	0
Valve	Gas/Vapor	0	0	0	0
	Light liquid	9	0	0	0.00252
	Heavy liquid	0	0	0	0
Flange	All	81	0	0	0.00162
				Total	0.00414
					2.98(kg/month) / 0.036 (Ton/Annum)

6. Total VOC emission from CHU measured in February 24:

No of points checked: 120

No of leaking (VOC>1ppm) points: 17

No of non leaking points: 103

	Number of S	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dumo	Light liquid	0	0	0	0
Pump	Heavy liquid	0	0	0	0
Valve	Gas/Vapor	0	0	0	0
	Light liquid	6	0	0	0.00168
	Heavy liquid	0	0	0	0
Flange	All	11	0	0	0.00022
				Total	0.0019
					1.37 (kg/month) / 0.016(Ton/Annum)

7. Total VOC emission from NCU measured in March 24:

No of points checked: 1194

No of leaking (VOC>1ppm) points: 235

No of non leaking points: 959

	Number of S	Computed Emission Estimates (EE)			
Source	Service	0-1000	1001-10000	Over 10,000	Per Source Type(kg/hr)
Dumn	Light liquid	2	0	0	0000396
Pump	Heavy liquid	0	0	0	0
	Gas/Vapor	3	0	0	0.00042
Valve	Light liquid	56	0	0	0.01568
	Heavy liquid	0	0	0	0
Flange	All	174	0	0	0.00348
				Total	0.02354
					16.95 (kg/month) / 0.203(Ton/Annum)

Reference: USEPA Handbook on Control Techniques for Fugitive VOC Emissions from Chemical Process Facilities. EPA/625/R-93/005, March 1994.

Page – 49